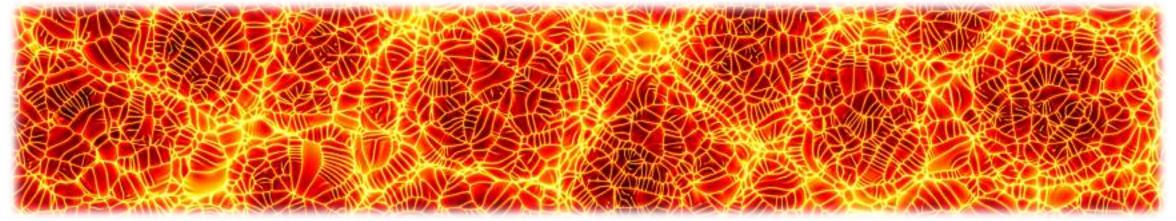
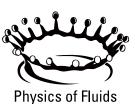
#### Computational Methods in Water Resources 2022

## Three-dimensional Rayleigh-Darcy convection at high Rayleigh numbers





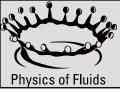


M. De Paoli<sup>1,2</sup>, F. Zonta<sup>2</sup>, S.Pirozzoli<sup>3</sup> & A. Soldati<sup>2,4</sup>

<sup>1</sup>Physics of Fluids Group, University of Twente, Enschede (The Netherlands)
<sup>2</sup>Institute of Fluid Mechanics and Heat Transfer, TU Wien, Vienna (Austria)
<sup>3</sup>Department of Aerospace and Mechanical Engineering, La Sapienza University, Rome, (Italy)
<sup>4</sup>Polytechnic Department, University of Udine, Udine (Italy)

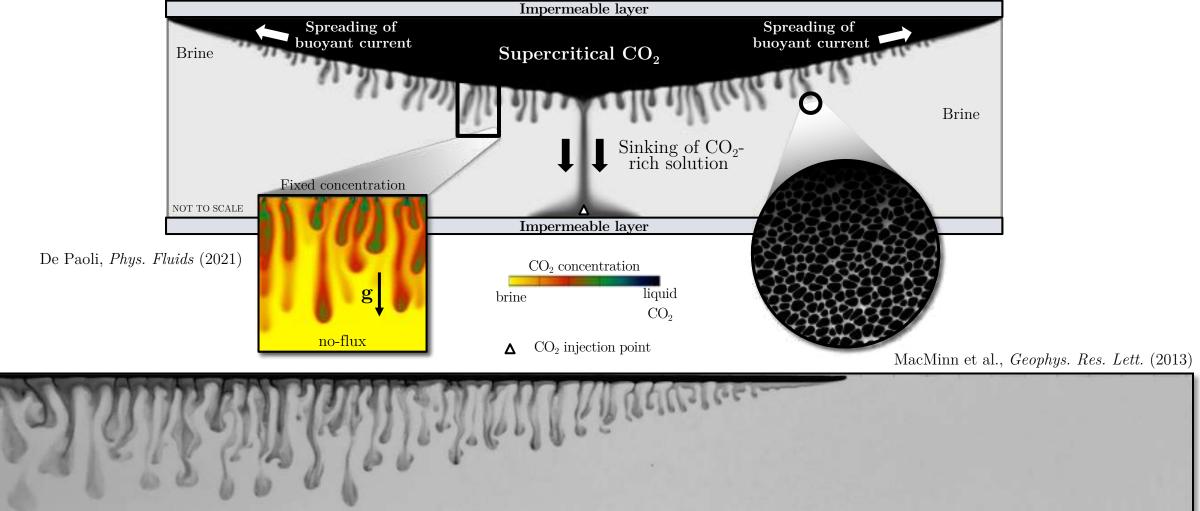


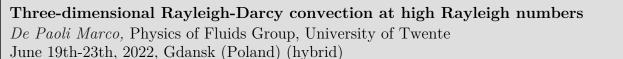




## Carbon Capture and Storage

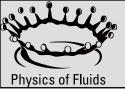






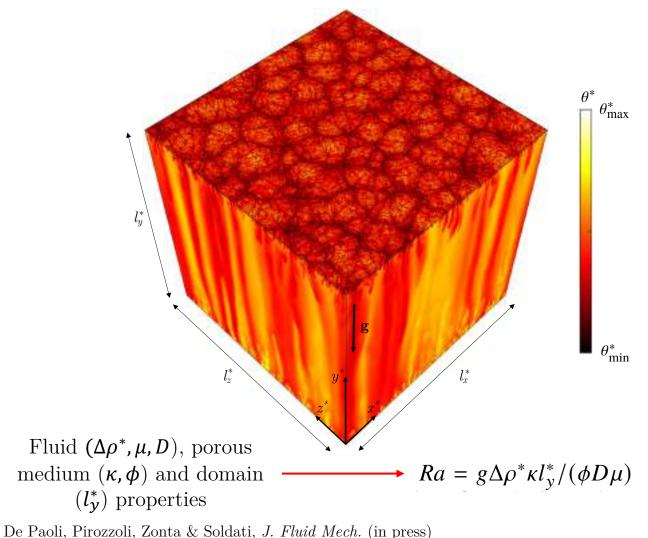


75x realtime



## Methodology





#### **Equations**

$$\frac{\partial \theta}{\partial t} + \nabla \cdot \left( \mathbf{u}\theta - \frac{1}{\mathrm{Ra}} \nabla \theta \right) = 0,$$

$$\nabla \cdot \mathbf{u} = 0$$
 ,  $\mathbf{u} = -(\nabla p - \theta \mathbf{j})$ ,

#### **Boundary conditions**

$$v(y = 0) = 0$$
 ,  $\theta(y = 0) = 1$ ,  
 $v(y = 1) = 0$  ,  $\theta(y = 1) = 0$ .

#### Simulations performed

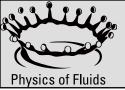
Simulation	Ra	$l_x/l_y \times l_z/l_y$	$N_x \times N_z \times N_y$
$Ra_1$	$1.0 \times 10^3$	4 × 4	$384 \times 384 \times 32$
$Ra_2$ $Ra_5$	$2.5 \times 10^3$ $5.0 \times 10^3$	$4 \times 4$ $4 \times 4$	$768 \times 768 \times 64$ $1536 \times 1536 \times 128$
$Ra_7$ $Ra_{10}$	$7.5 \times 10^3$ $1 \times 10^4$	$4 \times 4$ $1 \times 1$	$2304 \times 2304 \times 192$ $768 \times 768 \times 256$
$Ra_{20}$	$2 \times 10^4$ $3 \times 10^4$	1 × 1	$1536 \times 1536 \times 512$ $2304 \times 2304 \times 768$
$Ra_{40}$ $Ra_{80}$	$4 \times 10^4$ $8 \times 10^4$	1 × 1 1 × 1	$3072 \times 3072 \times 1024$ $6144 \times 6144 \times 2048$
$Ra_{10}$ $Ra_{20}$ $Ra_{30}$ $Ra_{40}$	$1 \times 10^4$ $2 \times 10^4$ $3 \times 10^4$ $4 \times 10^4$	1 × 1 1 × 1 1 × 1 1 × 1	$768 \times 768 \times 256$ $1536 \times 1536 \times 512$ $2304 \times 2304 \times 768$ $3072 \times 3072 \times 1024$



De Paoli Marco, Physics of Fluids Group, University of Twente June 19th-23th, 2022, Gdansk (Poland) (hybrid)

Pirozzoli, De Paoli, Zonta & Soldati, J. Fluid Mech. (2021)





#### Numerical details



- <u>Spatial discretization</u>: Second-order finite-difference incompressible flow solver (staggered arrangement of the flow variables, Orlandi, *Fluid Flow Phenomena*, 2000)
- <u>Time discretization</u>: the temperature transport equation is advanced in time by means of a hybrid third-order low-storage Runge–Kutta algorithm, whereby the convective terms are handled explicitly and the diffusive terms are handled implicitly, limited to the wall-normal direction.
- Pure MPI parallelization: Cineca Supercomputing centre, Infrastructure Marconi,

$$32,000 \text{ cores}$$
  $\approx 3\text{TB/field}$ 

De Paoli, Pirozzoli, Zonta & Soldati, J. Fluid Mech. (in press) Pirozzoli, De Paoli, Zonta & Soldati, J. Fluid Mech. (2021)

#### Equations

$$\frac{\partial \theta}{\partial t} + \nabla \cdot \left( \mathbf{u}\theta - \frac{1}{\mathrm{Ra}} \nabla \theta \right) = 0,$$

$$\nabla \cdot \mathbf{u} = 0 \quad , \quad \mathbf{u} = - \left( \nabla p - \theta \mathbf{j} \right),$$

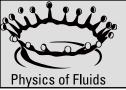
#### **Boundary conditions**

$$v(y = 0) = 0$$
 ,  $\theta(y = 0) = 1$ ,  
 $v(y = 1) = 0$  ,  $\theta(y = 1) = 0$ .

#### Simulations performed

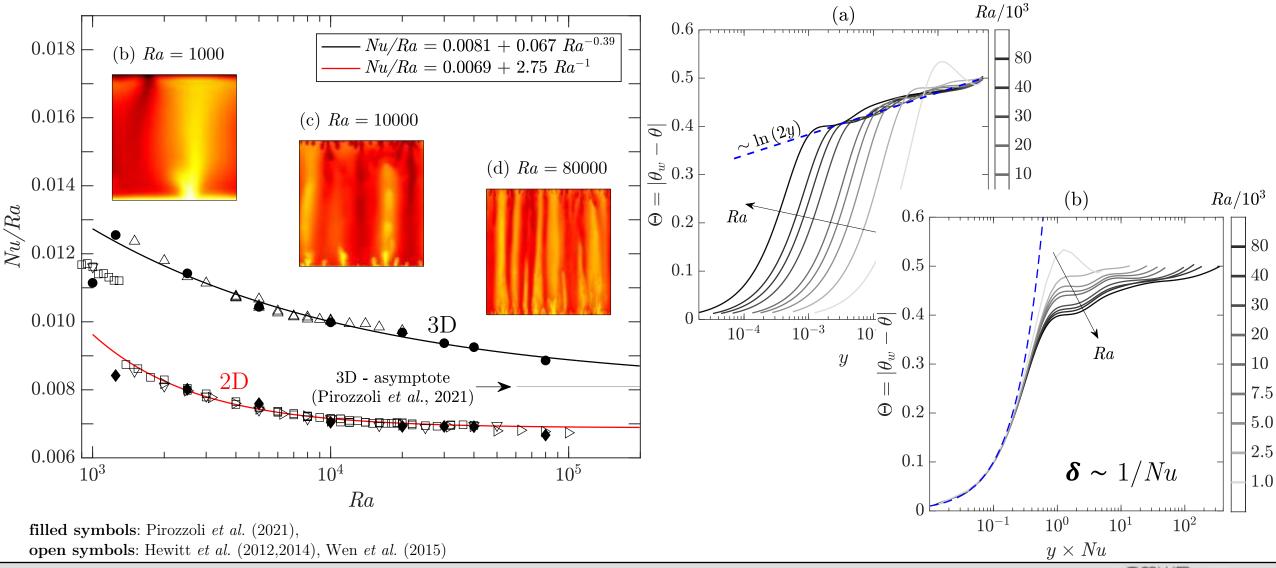
Simulation	Ra	$l_x/l_y \times l_z/l_y$	$N_x \times N_z \times N_y$
$Ra_1$	$1.0 \times 10^{3}$	$4 \times 4$	$384 \times 384 \times 32$
$Ra_2$	$2.5 \times 10^{3}$	$4 \times 4$	$768 \times 768 \times 64$
$Ra_5$	$5.0 \times 10^{3}$	$4 \times 4$	$1536 \times 1536 \times 128$
$Ra_7$	$7.5 \times 10^{3}$	$4 \times 4$	$2304 \times 2304 \times 192$
$Ra_{10}$	$1 \times 10^{4}$	$1 \times 1$	$768 \times 768 \times 256$
$Ra_{20}$	$2 \times 10^{4}$	$1 \times 1$	$1536 \times 1536 \times 512$
$Ra_{30}$	$3 \times 10^{4}$	$1 \times 1$	$2304 \times 2304 \times 768$
$Ra_{40}$	$4 \times 10^{4}$	$1 \times 1$	$3072 \times 3072 \times 1024$
$Ra_{80}$	$8 \times 10^{4}$	$1 \times 1$	$6144 \times 6144 \times 2048$





## Temperature and heat transfer statistics

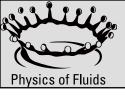




Three-dimensional Rayleigh-Darcy convection at high Rayleigh numbers

De Paoli Marco, Physics of Fluids Group, University of Twente June 19th-23th, 2022, Gdansk (Poland) (hybrid)

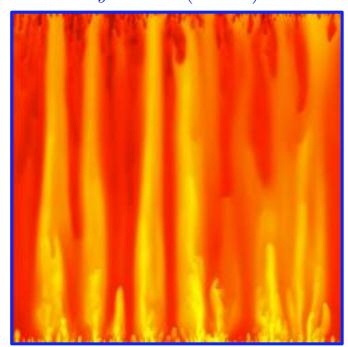


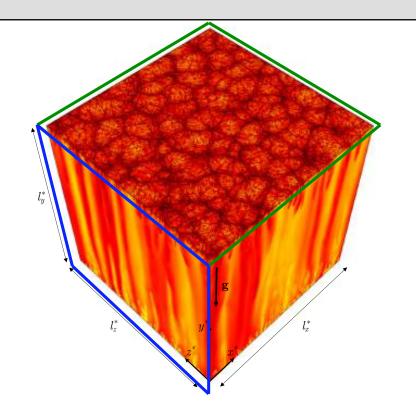


## Flow structure at high-Ra (Ra = $8 \times 10^4$ )

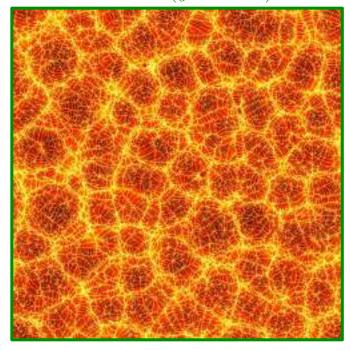


y-z slice (x = 0)

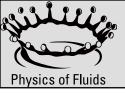




x-z slice (y = 0.01)

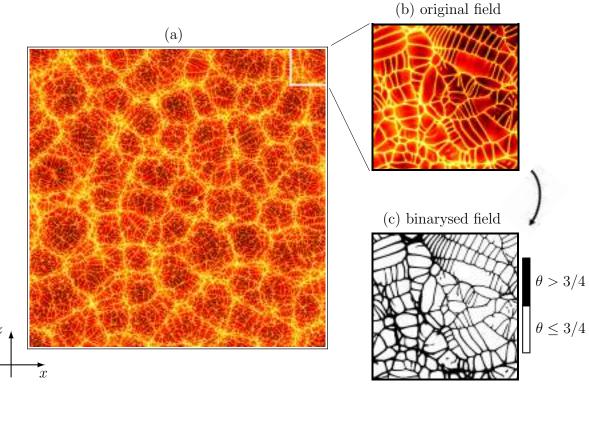


Pirozzoli, De Paoli, Zonta & Soldati, J. Fluid Mech (2021)



## Characterization of near-wall cell pattern



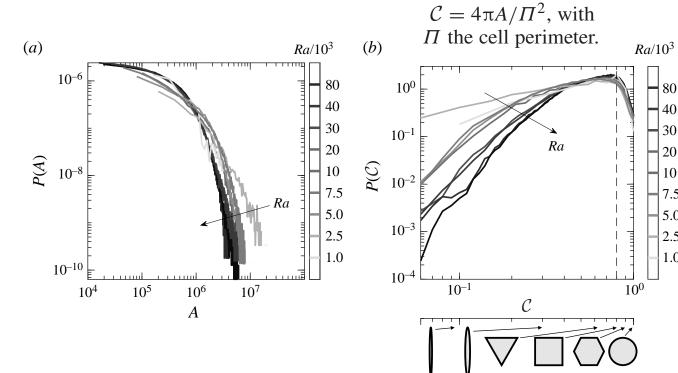


Near-wall temperature field binarization

De Paoli, Pirozzoli, Zonta & Soldati, J. Fluid Mech. (in press)

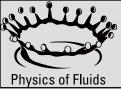
#### Characterization of cell pattern:

- Identification of cells area, A
- Identification of cells shape (circularity, C)



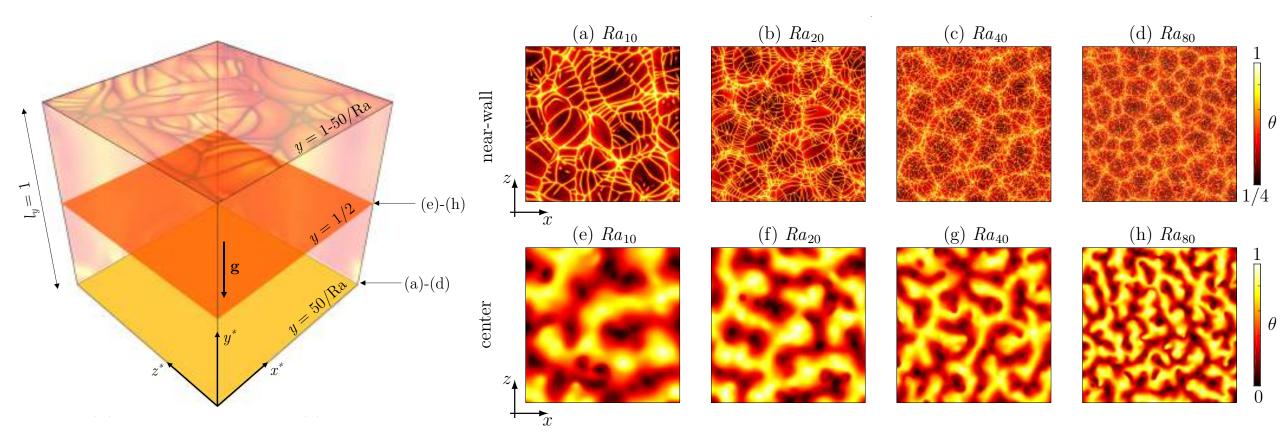






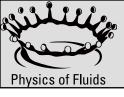
#### Near-wall and core flow





Are supercells correlated to megaplumes?

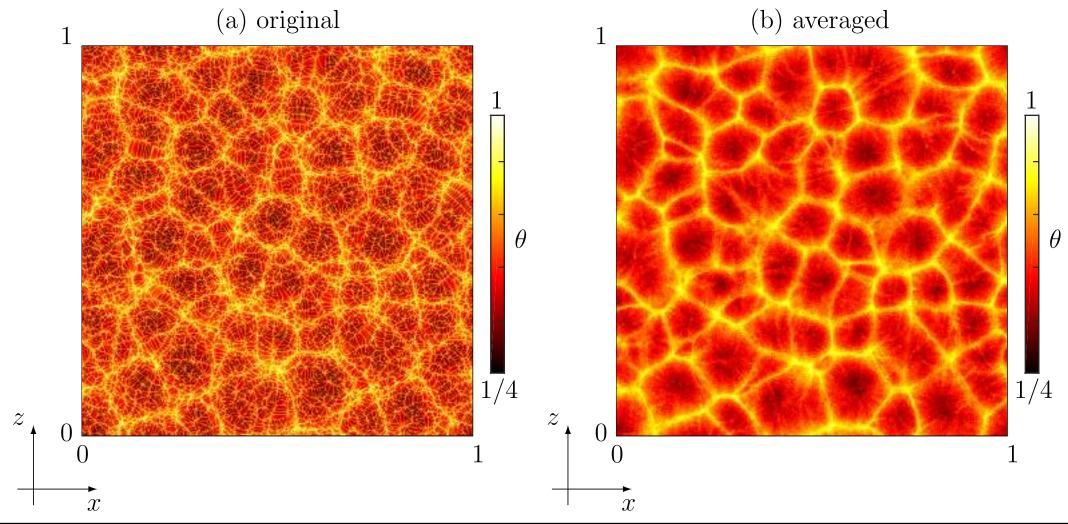


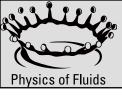


## Near-wall flow structures and supercells









## Near-wall and core flow



#### Mean radial wave number

$$\overline{k}_r(y) = \left\langle \frac{\int \int \sqrt{k_x^2 + k_z^2} E(k_x, k_z) \, dx dz}{\int \int E(k_x, k_z) \, dx dz} \right\rangle$$

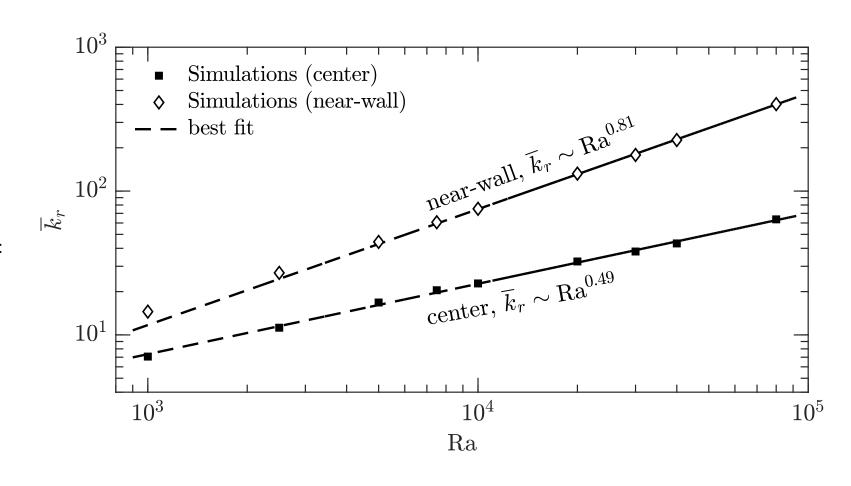
Theoretical prediction (Hewitt et al., 2014):

$$center$$

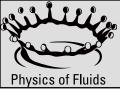
$$\overline{k}_r \sim Ra^{1/2}$$

near-wall

$$\overline{k}_r \sim \delta \sim 1/Nu$$



CMWF



## Supercells and megaplumes

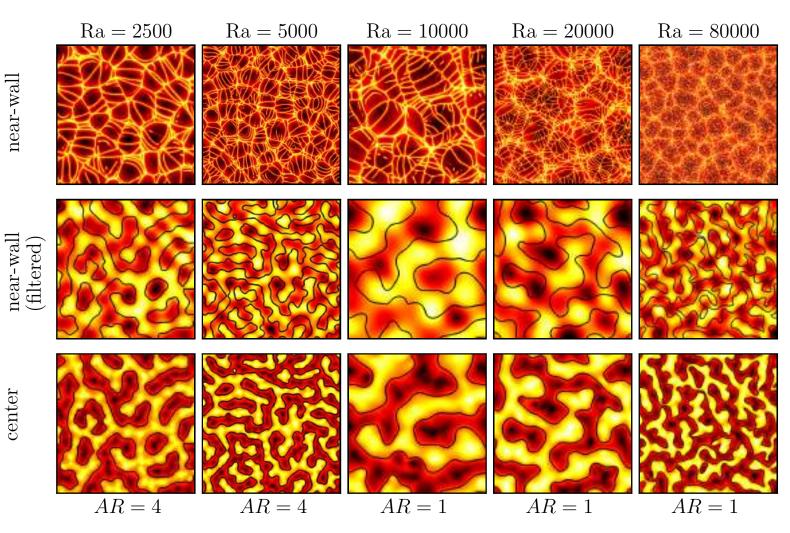


#### Mean radial wave number

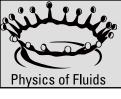
$$\overline{k}_r(y) = \left\langle \frac{\int \int \sqrt{k_x^2 + k_z^2} E(k_x, k_z) \, dx dz}{\int \int E(k_x, k_z) \, dx dz} \right\rangle$$

Following Berghout *et al.* (2021), we filter out the small-scale structures

Supercells are the footprint of megaplumes



CMWR



## Supercells and megaplumes

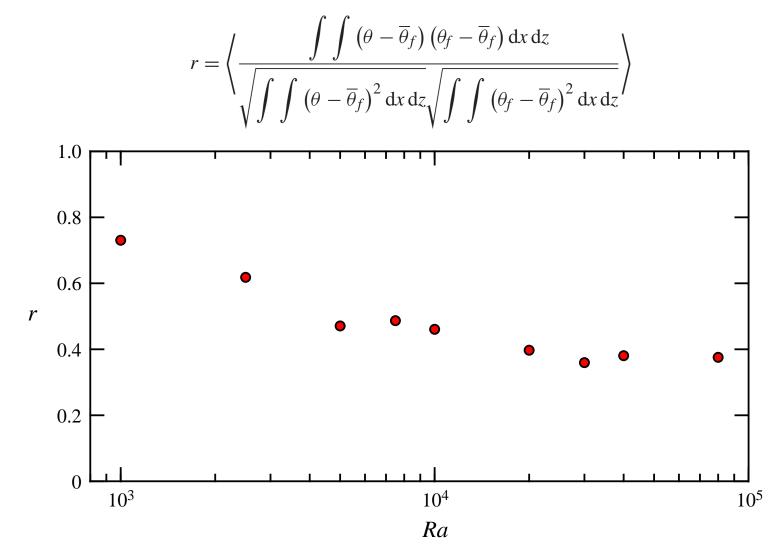


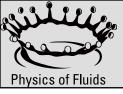
#### Mean radial wave number

$$\overline{k}_r(y) = \left\langle \frac{\int \int \sqrt{k_x^2 + k_z^2} E(k_x, k_z) \, dx dz}{\int \int E(k_x, k_z) \, dx dz} \right\rangle$$

Following Berghout *et al.* (2021), we filter out the small-scale structures

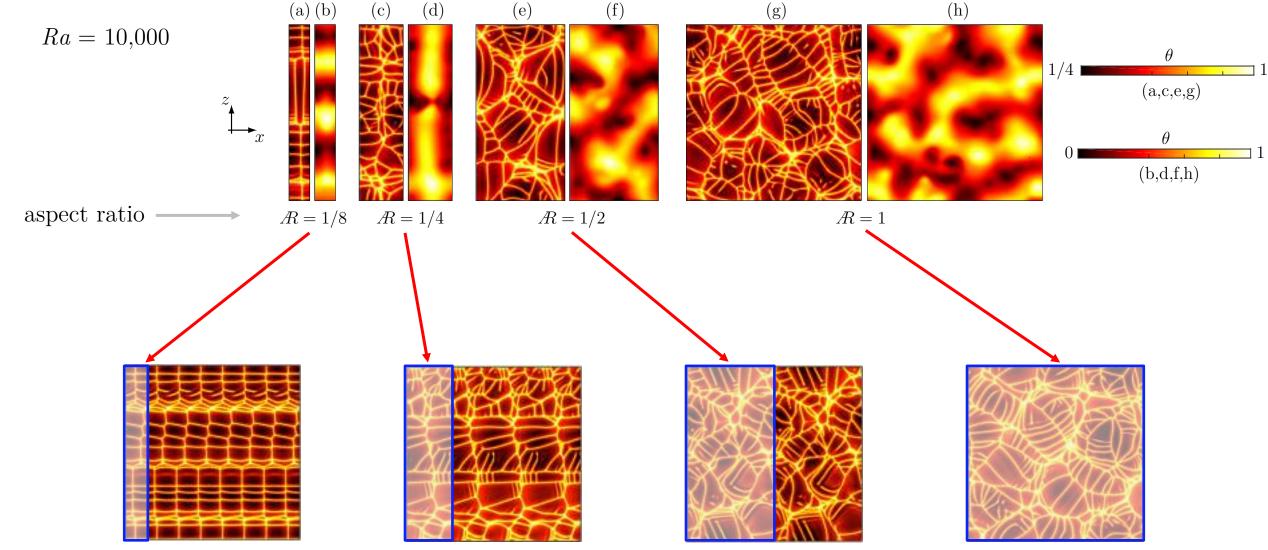
Supercells are the footprint of megaplumes

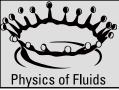




#### Assessment of domain size effects

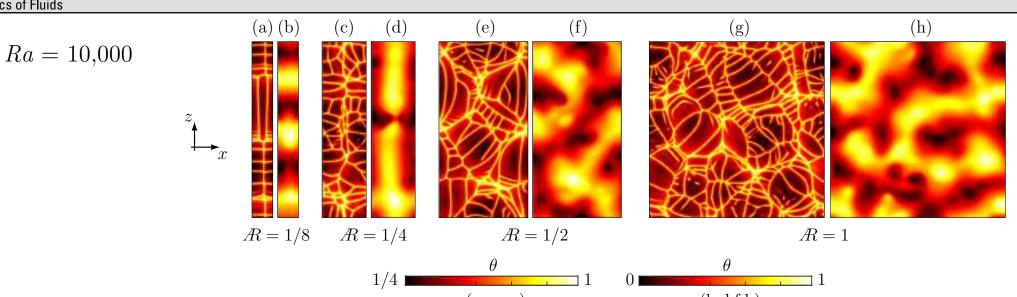




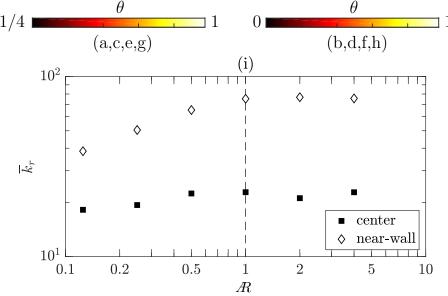


## Assessment of domain size effects

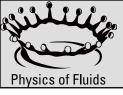




Also at large Ra [ $O(10^3)$ ], a minimum aspect ratio of 1 is required to accurately describe the large-scale flow structures

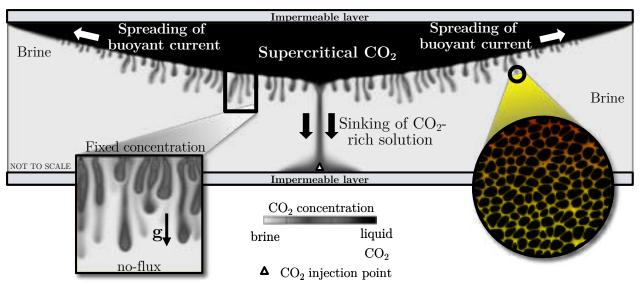




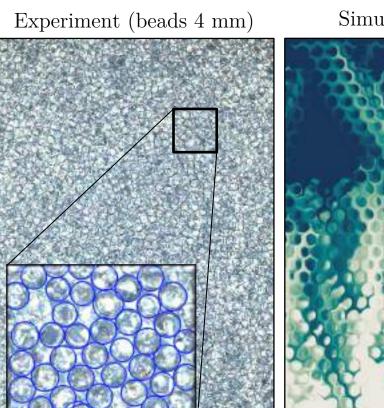


## Future developments – pore-scale dynamics





Numerical and experimental investigation of pore-scale dispersion effects on convective dissolution



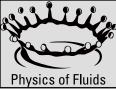
Simulations (IBM)



Chris Howland, *Physics of Fluids Group*, University of Twente

15







# Thank you for your attention! Questions?

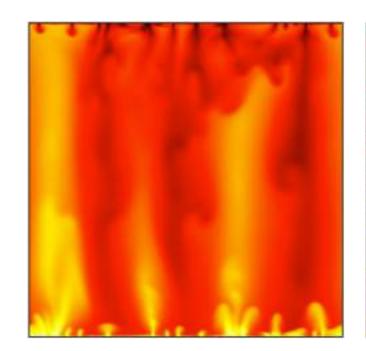
This research was funded in part by the Austrian Science Fund (FWF) [Grant J-4612]

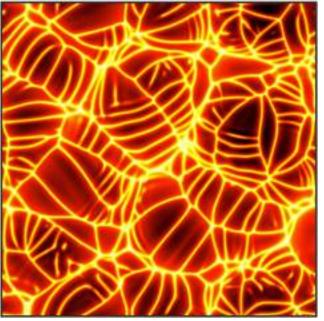


Der Wissenschaftsfonds.



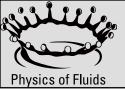
HPC resources provided by PRACE [Grant Pra21-5415]





Physics Today **74**, 5, 68 (2021)





## Additional numerical details



#### $\underline{Additional\ details\ on\ spatial\ discretization}$

- Wall-normal direction: hyperbolic tangent stretching function
  - Approximately 20 points within the thermal boundary layer
- Horizontal directions: uniform spacing
- Fourier expansion along the horizontal periodic directions yields a system of tridiagonal equations in the wall-normal direction for each Fourier mode, which is then solved with standard highly efficient numerical techniques

#### **Equations**

$$\frac{\partial \theta}{\partial t} + \nabla \cdot \left( \mathbf{u}\theta - \frac{1}{\mathrm{Ra}} \nabla \theta \right) = 0,$$

$$\nabla \cdot \mathbf{u} = 0$$
 ,  $\mathbf{u} = -(\nabla p - \theta \mathbf{j})$ ,

#### Boundary conditions

$$v(y = 0) = 0$$
 ,  $\theta(y = 0) = 1$ ,  $v(y = 1) = 0$  ,  $\theta(y = 1) = 0$ .

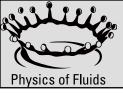
The pressure field is determined by solving the Poisson equation resulting from the divergence-free constraint:

$$\nabla^2 p = \frac{\partial \theta}{\partial y}$$

$$\partial p/\partial y = 0$$
 at walls (no-penetration)

De Paoli, Pirozzoli, Zonta & Soldati, J. Fluid Mech. (in press) Pirozzoli, De Paoli, Zonta & Soldati, J. Fluid Mech. (2021)

17





High-resolution images, movies and slides are available upon request to <a href="mailto:m.depaoli@utwente.nl">m.depaoli@utwente.nl</a>

